

## Chemical Reactor Analysis and Design Fundamentals

### 2nd Edition

#### Errata for Second Edition, Second Printing

March 20, 2018

1. p. 103, third line from bottom. Change  $\pi(n - 1)$  to  $\pi(n + 1)$ .
2. pp. 205–207, Example 5.1. Replace all occurrences of “oxirane” with “trioxane.” Thanks to Travis Arnold of UW for pointing out this erratum.
3. pp. 405–407, Example 7.6. The rate constant should be  $k = 1.3828 \times 10^{19} \exp(-13,500/T)$ . The flowrate should be  $Q_f = 792$  L/s. With the adjusted rate constant and flowrate given above, the reactor volume should be  $V_R = 233$  cm<sup>3</sup> instead of L. Also change the units on the x-axis from L to cm<sup>3</sup> in Figures 7.27 and 7.28. Thanks to Jason Haugh and the students at NC State for reporting this erratum. See also Exercise 7.21.
4. p. 405, seventh line from bottom. Replace “The catalyst pellet radius is 0.1 cm.” with, “The spherical catalyst pellet radius is 0.1 cm, and the densities are  $\rho_p = 0.68$ ,  $\rho_B = 0.60$  g/cm<sup>3</sup>.”
5. p. 416, 11th line, change “bulk fluid density” to “bulk fluid viscosity.”
6. p. 426, Exercise 7.21. The rate constant should be  $k = 1.3828 \times 10^{19} \exp(-13,500/T)$ . The flowrate should be  $Q_f = 792$  L/s. See also Example 7.6.
7. p. 553. Change concentration (kmol/dm<sup>3</sup>) to total amount (kmol) in y-axis labels and captions of Figures 9.33 and 9.34. Change figure labels  $c_j$  to  $n_j$ . Thanks to Joel Andersson of UW for pointing out this erratum.